

# Temperature and humidity dependence of secondary organic aerosol yield from the ozonolysis of $\beta$ -pinene\*

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Received: 15 January 2007 – Accepted: 23 January 2007 – Published: 14 February 2007

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\*Invited contribution by C. Stenby, one of the EGU Outstanding Young Scientist Award winners 2005.

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## Abstract

The temperature dependence of secondary organic aerosol (SOA) formation from ozonolysis of  $\beta$ -pinene was studied in a flow reactor at 263 K–303 K and 1007 hPa under dry and humid conditions (0% and 26%–68% relative humidity, respectively).

5 The observed SOA yields were of similar magnitude as predicted by a two-product model based on detailed gas phase chemistry (Jenkin, 2004), reaching maximum values of 0.18–0.39 at high particle mass concentrations ( $M_o$ ). Under dry conditions, however, the measurement data exhibited significant oscillatory deviations from the predicted linear increase with inverse temperature (up to 50% at high  $M_o$ ). Under hu-

10 mid conditions the SOA yield exhibited a linear decrease with inverse temperature, which is opposite to modelled temperature dependence and implies that the model substantially overestimates the yield at low temperatures and underestimates it at high temperatures (deviations up to 80% at high  $M_o$ ). For the atmospherically relevant concentration level of  $M_o = 10 \mu\text{g m}^{-3}$  and temperature range 263 K–293 K, the results from

15 humid experiments in this study indicate that the SOA yield of  $\beta$ -pinene ozonolysis may be well represented by an average value of 0.15 with an uncertainty estimate of  $\pm 0.05$ . When fitting the measurement data with a two-product model, both the partitioning coefficients ( $K_{om,i}$ ) and the stoichiometric yields ( $\alpha_i$ ) of the low-volatile and semi-volatile model species were found to vary with temperature. The results indicate

20 that not only the reaction product vapour pressures but also the relative contributions of different gas-phase or multiphase reaction channels are strongly dependent on temperature and the presence of water vapour. In fact, the oscillatory positive temperature dependence observed under dry conditions and the negative temperature dependence observed under humid conditions indicate that the SOA yield is governed much more

25 by the temperature and humidity dependence of the involved chemical reactions than by vapour pressure temperature dependencies. We suggest that the elucidation and modelling of SOA formation need to take into account the effects of temperature and humidity on the pathways and kinetics of the involved chemical reactions as well as on

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the gas-particle partitioning of the reaction products.

## 1 Introduction

Atmospheric aerosol particles affect the atmosphere and climate by absorption and scattering of radiation, by influencing the formation and properties of clouds and precipitation, and by heterogeneous chemical reactions (Fuzzi et al., 2006). We study secondary organic aerosols (SOA) from the ozonolysis of the biogenic volatile organic compound (BVOC)  $\beta$ -pinene, because  $\beta$ -pinene is very abundant and simulations have shown that the particles are likely to be important as CCN (Tunved et al., 2006). Forests and other vegetation emit large amounts of BVOCs ( $500\text{--}1800\text{ Tg C a}^{-1}$ ), which are oxidised in the atmosphere primarily by  $\text{O}_3$ , OH and  $\text{NO}_3$  radicals. Biogenic SOA are formed when low volatile oxidation products condense on pre-existing particles or newly formed particles. Second to isoprene, monoterpenes are the most abundant BVOCs and they are usually assumed to account for most if not all SOA formation in current state-of-the-art models of global atmospheric chemistry (Kanakidou et al., 2005). With an emission rate of  $10\text{--}50\text{ Tg C a}^{-1}$ ,  $\beta$ -pinene is the second most important monoterpene (Wiedinmyer et al., 2004). Recent laboratory studies demonstrated the ability of SOA from monoterpenes to act as cloud condensation nuclei (Hartz et al., 2005; VanReken et al., 2005).

The temperature dependence of SOA formation from ozonolysis has recently been modelled by Sheehan and Bowman (2001), and their parameterization has been incorporated into some advanced global atmospheric chemistry models (Chung and Seinfeld, 2002; Tsigaridis and Kanakidou, 2003). Nevertheless, these models appear to underestimate the organic aerosol particle mass in the free troposphere, which may be due to shortcomings in the characterization and representation of the temperature dependence of SOA formation (Heald et al., 2005). To our knowledge only one experimental study has addressed this issue up to now: Takekawa et al. (2003) reported a twofold increase of the SOA yield from ozonolysis of  $\alpha$ -pinene at 283 K compared to

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303 K, but they investigated no other temperatures or monoterpenes. For SOA formation from the ozonolysis of  $\beta$ -pinene, Jenkin (2004) has presented a two-product model based on a detailed gas phase chemical mechanism (Sect. 2.7.2).

Water vapour has been found to reduce the particle volume concentration from ozonolysis of  $\beta$ -pinene (Bonn et al., 2002), but to increase or not affect the SOA yield from other monoterpenes (Cocker et al., 2001; Jonsson et al., 2006). The decrease in particle volume concentration for  $\beta$ -pinene has been attributed to the reaction of water vapour with the stabilized  $C_9$ -Criegee Intermediate ( $C_9-CI_{stab}$ ) which increases the production of nopinone and hydrogenperoxide that are not condensing (Winterhalter et al., 2000):

Reaction 2a competes with the reaction of  $C_9-CI_{stab}$  with carbonyl compounds (aldehydes or ketones) producing secondary ozonides (Reaction 2b), that are presumably important for new particle formation (Bonn et al., 2002). The increase of SOA yield in the presence of water vapour observed for other monoterpenes cannot be explained by the physical growth by uptake of water (Jonsson et al., 2006), but no chemical mechanisms have been proposed yet.

For the elucidation, development, and evaluation of SOA formation mechanisms and model parameterizations we have experimentally investigated the temperature dependence of the SOA yield from the ozonolysis of  $\beta$ -pinene under both dry and humid conditions.

## 2 Methods

### 2.1 Preparation of the reactants

Ozone was generated by irradiating a flow of synthetic air (79.5%  $N_2$  and 20.5%  $O_2$ , Air Liquide or Westfalen) mixed with nitrogen (99.999%  $N_2$ , Air Liquide or Westfalen) with the UV light from a mercury Pen-Ray lamp. The volume mixing ratio of ozone was controlled by varying the ratio of synthetic air to nitrogen. The concentration of ozone

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was monitored by UV absorption at  $\lambda=254$  nm and calibrated with a commercial ozone monitor (Model 202, 2B Technologies, Inc.) mounted at the outlet of the flow reactor to account for wall loss of ozone.

$\beta$ -Pinene (99.5%) was obtained from Sigma-Aldrich Chemical Co and used as received. It is a liquid with a vapour pressure of 313 Pa at 293 K. The gas mix of  $\beta$ -pinene in nitrogen was prepared by evaporating pure  $\beta$ -pinene into an evacuated steel vessel ( $V=14.67$  l) and adding nitrogen to a pressure of about 6000 hPa; the  $\beta$ -pinene concentrations were measured with long-path FTIR spectroscopy.

## 2.2 Aerosol formation

Figure 1 displays a schematic drawing of the experimental set-up applied in this study (described in detail by Bonn et al., 2002). The SOA formation experiments were performed in a vertical flow tube reactor (120 cm length, 10 cm inner diameter, Pyrex glass walls), operated with a laminar gas flow of  $5$  l  $\text{min}^{-1}$  and a center velocity of  $2$  cm  $\text{s}^{-1}$  (Bonn et al., 2002). All flows were controlled by MKS mass flow controllers. The temperature was taken into account when converting the volume flow to the mass flow of the flow controllers. The flow of synthetic air and ozone from the Pen-Ray lamp ( $0.2$  l  $\text{min}^{-1}$ ) was mixed with nitrogen to  $2.0$  l  $\text{min}^{-1}$  and introduced through the center of the inlet mixing plunger.  $\beta$ -pinene from the pressurized steel vessel was mixed with synthetic air to a flow of  $3$  l  $\text{min}^{-1}$  and introduced at the top of the flow reactor. For the experiments under humid conditions the synthetic air was humidified by passage over liquid water in a thermostatted vessel, before mixing with the  $\beta$ -pinene flow. The temperature of the vessel was adjusted in the range 293 K–323 K to establish 26%–68% relative humidity (RH) in the flow reactor, which was measured by a dew-point meter (Panametrics, Moisture Monitor Series 35) at the excess flow outlet. To avoid damage of the dew-point meter, RH was only measured in the beginning and end of each experiment, when the air was free of particles. In the dry experiments test measurements showed that  $\text{RH} < 0.03\%$ . The two flows containing ozone and  $\beta$ -pinene were mixed under turbulent conditions in the movable inlet mixing plunger. The reaction time ( $\Delta t$ ) was

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controlled by adjusting the distance between plunger and outlet. In the experiments reported here, the distance was kept at 80 cm, to assure that the reactants reached the temperature of the flow reactor before being mixed, while having a maximized reaction time allowing minimal reactant concentrations. The amount of reacted  $\beta$ -pinene was varied by varying the initial volume mixing ratios of  $\beta$ -pinene and ozone over the range of 0.6 ppmv–10.9 ppmv and 0.2 ppmv–2.4 ppmv respectively. The amount reacted was 0.4%–3.9% ( $31 \mu\text{g m}^{-3}$ – $1273 \mu\text{g m}^{-3}$ ) for  $\beta$ -pinene and 0.5%–14.6% for ozone.

### 2.3 Aerosol analysis

Number size distributions of the particles formed in the flow reactor were measured with a scanning mobility particle sizer (SMPS) system (Model 3936, TSI Inc.) with a long differential mobility analyzer (LDMA, Model 3081, TSI Inc.) and ultrafine condensation particle counter (UCPC, Model 3025A, TSI Inc.). The sampling flow rate was  $0.3 \text{ l min}^{-1}$ , and the position of the sampling orifice with a radius of 1.1 cm was radially centered about 3 cm above the bottom of the flow reactor. Compared to the reaction time in the flow tube (40 s), the additional time in the neutralizer was negligible ( $<1$  s). The DMA sheath air flow rate was varied between 3 and  $9.7 \text{ l min}^{-1}$  (see Table 1) to optimize the relation between the detectable size range and the diffusional loss of the small particles. A few tests showed that the yield was not affected by the change in sheath air flow rate. The sheath air flow was regulated with a mass flow controller, and the temperature used for conversion of mass to volume flow rate was measured where the sheath air enters the DMA. To minimize ozonolysis inside the DMA, an ozone scrubber consisting of a glass tube filled with silver wool was installed in the sheath air loop, reducing the ozone concentration to less than the limit of detection (2 ppbv). Due to the ten-fold or higher dilution of the sample flow with ozone-free sheath air and short residence time (1.5 s), ozonolysis reactions in the DMA were negligible. The silver wool may also have scrubbed reaction products from the gas phase, but we assume that equilibrium was re-established when the sheath air was flowing through the filter collecting the SOA particles. For the humid experiments the sheath

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air was pre-conditioned for a couple of hours to ensure stable conditions throughout the system.

For each experiment the flow reactor and the SMPS system were kept at a common temperature (within  $\pm 2$  K), by circulating ethanol/water through glass/steel jackets and through a hose wrapped around the DMA as illustrated in Fig. 1. A Julabo F20 cryostat combined with a Julabo FT 401 cooler was used for the flow reactor and the aerosol neutraliser, and a MGW Lauda RM6 cryostat for the DMA and its sheath air loop. Note that warm and humid conditions in the laboratory can lead to water condensation and short circuiting of the cooled DMA, which can be avoided by using only low voltages of the DMA.

In every SOA formation experiment, the number size distribution measurements were repeated 4–24 times. Conditions and results of the individual experiments are summarized in Table 1 for the dry experiments and Table 2 for the humid experiments.

## 2.4 Data analysis

SOA formation yields ( $Y$ ) were calculated as the ratio of the mass concentration of secondary organic particulate matter ( $M_o$ ) to the decrease of  $\beta$ -pinene mass concentration ( $-\Delta[\beta\text{-pinene}]$ ):

$$Y = \frac{M_o}{-\Delta[\beta\text{-pinene}]} \quad (1)$$

$M_o$  was calculated from the average of the measured mobility equivalent aerosol number size distributions, assuming compact spherical particles with an effective density of  $1.2 \text{ g cm}^{-3}$  (Bahreini et al., 2005).  $M_o$  obtained under humid conditions ( $M_{o,\text{humid}}$ ) was corrected as follows to exclude the influence of water vapour uptake on particle size:

$$M_o = \frac{M_{o,\text{humid}}}{GF^3} \quad (2)$$

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$$GF = \frac{D_{p,wet}}{D_{p,dry}} \quad (3)$$

$GF$  is the growth factor and  $D_p$  is the particle diameter. Varutbangkul et al. (2006) have reported the dependency of  $GF$  for SOA particles from  $\beta$ -pinene ozonolysis on relative humidity (RH):

$$GF = 1 + \left[ \left( 1 - \frac{RH}{100\%} \right)^{-0.5108} 0.0367 \left( \frac{RH}{100\%} \right)^{1.5177} \right] \quad (4)$$

We assume that this dependency is independent of temperature.

For the determination of  $-\Delta[\beta\text{-pinene}]$  we calculated the decrease of ozone concentration ( $-\Delta[O_3]$ ) assuming pseudo-first order reaction kinetics based on a near-constant excess concentration of  $\beta$ -pinene ( $[\beta\text{-pinene}]_0$ ):

$$-\Delta[O_3] = [O_3]_0 * \left( 1 - \exp(k_{O_3} [\beta\text{-pinene}]_0 \Delta t) \right) \quad (5)$$

$$-\Delta[\beta\text{-pinene}] = 1.35 (-\Delta[O_3]) \quad (6)$$

The factor of 1.35 was applied because the ozonolysis of  $\beta$ -pinene produces OH radicals with a stoichiometric yield ( $\alpha_{OH}$ ) of 0.35 at 296 K (Atkinson et al., 1992). We assumed that  $\alpha_{OH}$  was independent of temperature (Atkinson, Personal communication), that OH was in steady state ( $k_{OH} = 7.89 \times 10^{-11} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1} \gg k_{O_3} = 1.5 \times 10^{-17} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$  at 298 K (Atkinson, 1994)) and that all OH radicals reacted with  $\beta$ -pinene which is supported by the large excess of  $\beta$ -pinene compared to its reaction products ( $-\Delta[\beta\text{-pinene}]/[\beta\text{-pinene}]_0 < 4\%$ ). For the few experiments where  $[O_3]_0$  was higher than  $[\beta\text{-pinene}]_0$ ,  $-\Delta[\beta\text{-pinene}]$  was calculated from Eq. (5) interchanging  $\beta$ -pinene and ozone. Temperature-dependent reaction rate coefficients ( $k_{O_3}$ ) were calculated from the Arrhenius equation:

$$k_{O_3} = A \exp\left(\frac{-E_a}{RT}\right) \quad (7)$$

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where  $A = 1.2 \times 10^{-15} \pm 4.6 \times 10^{-17} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$ ,  $E_a/R = 1300 \pm 75 \text{ K}$  (Khamaganov and Hites, 2001; Atkinson and Arey, 2003).

Standard deviations of  $M_o$  ( $s_{M_o}$ ) were calculated from repeated measurements of the SOA number size distribution. The number of measured size distributions (n) in each experiment is given in Tables 1 and 2. The standard deviation of the yield ( $s_Y$ ) was calculated by propagating  $s_{M_o}$  and the standard deviation of  $-\Delta[\beta\text{-pinene}]$  ( $s_{-\Delta\beta\text{-pinene}}$ ):

$$s_Y = Y * \sqrt{\left(\frac{s_{M_o}}{M_o}\right)^2 + \left(\frac{s_{-\Delta[\beta\text{-pinene}]}}{-\Delta[\beta\text{-pinene}]}\right)^2} \quad (8)$$

$s_{-\Delta\beta\text{-pinene}}$  was calculated from the standard deviations of  $\alpha_{\text{OH}}$ ,  $[\text{O}_3]_0$ ,  $[\beta\text{-pinene}]_0$ ,  $\Delta t$  and  $k_{\text{O}_3}$ :

$$s_{-\Delta[\beta\text{-pinene}]} = (-\Delta[\beta\text{-pinene}]) * \sqrt{\left(\frac{s_{\alpha_{\text{OH}}}}{\alpha_{\text{OH}}}\right)^2 + \left(\frac{s_{[\text{O}_3]_0}}{[\text{O}_3]_0}\right)^2 + \left(\frac{s_{k_{\text{O}_3}}}{k_{\text{O}_3}}\right)^2 + \left(\frac{s_{\Delta t}}{\Delta t}\right)^2 + \left(\frac{s_{[\beta\text{-pinene}]_0}}{[\beta\text{-pinene}]_0}\right)^2} \quad (9)$$

## 2.5 Two-product model

The ozonolysis of  $\beta$ -pinene generates a large variety of reaction products (Winterhalter et al., 2000). Commonly the products of this and other SOA formation reactions are lumped into low-volatile and semi-volatile species, and a two-product model is used to simulate the SOA yield from smog chamber data (Odum et al., 1996):

$$Y = M_o \left( \frac{\alpha_1 K_{om,1}}{R_{s,1} + K_{om,1} M_o} + \frac{\alpha_2 K_{om,2}}{R_{s,2} + K_{om,2} M_o} \right) \quad (10)$$

$K_{om,i}$  stands for the gas-particle partitioning coefficients,  $\alpha_i$  is the stoichiometric yield and  $R_{s,i}$  is the mass fraction of particulate matter that remains suspended in the gas. The counting variable  $i$  designates low volatile species (2) and semi-volatile species (2), respectively. During the short residence time in the flow reactor, the sampled aerosol does practically not interact with the walls, and thus we assume  $R_{s,i} = 1$ . For any wall

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loss to occur the particles in the sample flow would have to migrate by Brownian diffusion over a distance of 3.9 cm from the radially centered sampling orifice to the walls. For the smallest detected particles with a diameter of 8 nm, the probability for displacement larger than 0.4 cm within 40 s is only 0.3%. In contrast, the particle residence times in smog chamber experiments are typically on the order of hours, which leads to significant wall losses and  $R_{s,i} < 1$ .

## 2.6 Fitting procedures

### 2.6.1 “B fit”

Non-linear robust fits (Huber, 1981) of Eq. (10) to the experimental data pairs of  $M_o$  and  $Y$  were performed. The input parameters  $K_{om,1,303K}$  and  $K_{om,2,303K}$  were varied from  $0.001 \text{ m}^3 \mu\text{g}^{-1}$  to  $0.2 \text{ m}^3 \mu\text{g}^{-1}$  in steps of  $0.001 \text{ m}^3 \mu\text{g}^{-1}$  with the premise that  $K_{om,1,303K} > K_{om,2,303K}$ . The temperature dependence of  $K_{om,i}$  was derived from the Clausius-Clayperon equation describing the temperature dependence of the vapour pressure (Sheehan and Bowman, 2001):

$$K_{om,i,T} = K_{om,i,303K} \frac{T}{303 \text{ K}} \exp \left[ B_i \left( \frac{1}{T} - \frac{1}{303 \text{ K}} \right) \right] \quad (11)$$

$$B_i = \frac{\Delta_{\text{vap}} H_i}{R} \approx \frac{\Delta_{\text{vap}} S_i * T_{b,i}}{R} \quad (12)$$

$B$  values for the products from the  $\beta$ -pinene ozonolysis were calculated with the values of  $\Delta_{\text{vap}} S_i$ ,  $T_{b,i}$  and  $\alpha$  reported by Jenkin (2004) for nopinone, pinalic-3-acid and pinic acid. Jenkin (2004) also reported  $\alpha$  for acetone and formaldehyde, which were assumed to have the same  $\Delta_{\text{vap}} S_i$  and  $T_{b,i}$  as nopinone. The two acids were lumped as the low volatile species (1) and the three other compounds were lumped as the semi-volatile species (2) using the method of Bian and Bowman (2002) which led to

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$B_1=6153\text{ K}$  and  $B_2=5032\text{ K}$ . Start values of  $\alpha_1$  and  $\alpha_2$  were determined by test calculations (Table 3), and for each temperature  $\alpha_1$  and  $\alpha_2$  were optimized with a Nelder-Mead algorithm (Nelder and Mead, 1965) to minimize the residual parameter  $S_T$ :

$$S_T = \sum_j \frac{|Y_{\text{data},T} - Y_{\text{model},T}|_j}{S_{Y,\text{data},T,i}} \quad (13)$$

- 5 Best fit values of  $K_{om,1,303\text{ K}}$  and  $K_{om,2,303\text{ K}}$  were taken at the minimum of the sum of residual parameters  $\Sigma S_T$ .

### 2.6.2 “Free fit”

To investigate how the fit values change without constraints on the temperature dependence the data sets obtained at different temperatures have been fitted independently  
 10 by varying the input parameters  $K_{om,1}$  and  $K_{om,2}$  from  $0.001\text{ m}^3\mu\text{g}^{-1}$  to  $0.8\text{ m}^3\mu\text{g}^{-1}$  with steps of  $0.001\text{ m}^3\mu\text{g}^{-1}$ . For the data from experiments at  $263\text{ K}$  (dry and humid) and  $278\text{ K}$  (dry) it was necessary to raise the upper limit to  $100\,000\text{ m}^3\mu\text{g}^{-1}$  (steps of  $10\text{ m}^3\mu\text{g}^{-1}$ ),  $300\text{ m}^3\mu\text{g}^{-1}$  (steps of  $1\text{ m}^3\mu\text{g}^{-1}$ ) and  $3.150\text{ m}^3\mu\text{g}^{-1}$  (steps of  $0.001\text{ m}^3\mu\text{g}^{-1}$ ) respectively. Start values of  $\alpha_1$  and  $\alpha_2$  were not changed (Table 3).  
 15 The  $\alpha_i$  best-fit values were not correlated with the start values, confirming that fitting results were not biased by the start values.

## 2.7 Earlier investigations

### 2.7.1 Experimental studies

Five experimental studies on the aerosol yield of  $\beta$ -pinene ozonolysis have to our  
 20 knowledge been published. They have been conducted in static smog chambers under different experimental conditions as summarised in Table 4, but none of them covered a temperature and humidity range wider than a few K and few % RH, respectively.

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Most of the previous studies used seed aerosols, which are assumed to affect measurements of SOA yield only at very low particle number and mass concentrations (kinetic limitations of particle nucleation and growth). The lowest particle number and mass concentrations measured in our experiments were  $3.4 \times 10^5 \text{ cm}^{-3}$  and  $1.9 \mu\text{g m}^{-3}$ , which should be sufficiently high to avoid kinetic limitations and ensure comparability with earlier studies using seed aerosols.

OH scavengers are usually applied to investigate the reaction mechanism of alkene ozonolysis, but they are known to perturb SOA yield measurements. The extent and direction of perturbation depend on the type of alkene and OH scavenger (Docherty and Ziemann, 2003; Keywood et al., 2004). Griffin et al. (1999) and Yu et al. (1999) applied 2-butanol as an OH scavenger, which has been found to reduce the SOA yield from  $\beta$ -pinene ozonolysis substantially (Keywood et al., 2004). Lee et al. (2006) applied cyclohexane for OH scavenging, which has been found not to affect the SOA yield from  $\beta$ -pinene ozonolysis significantly (Docherty and Ziemann, 2003). To avoid perturbations and simulate atmospherically relevant conditions, no OH scavenger was applied in this study.

Most of the earlier studies assumed a particle density of  $1 \text{ g cm}^{-3}$ , only Lee et al. (2006) assume  $1.25 \text{ g cm}^{-3}$ . We assume a particle density of  $1.2 \text{ g cm}^{-3}$  based on Bahreini et al. (2005). Two of the previous studies reported fit-parameters for a one- or two-product model of SOA formation (Hoffmann et al., 1997; Griffin et al., 1999).

### 2.7.2 Model studies

Jenkin (2004) has presented a two-product model based on a detailed gas phase chemical mechanism and experimental investigations. He assumed a particle density of  $1 \text{ g cm}^{-3}$ , which is expected to lower the yield compared to our assumption of  $1.2 \text{ g cm}^{-3}$ . On the other hand, the simulations include the presence of cyclohexane as an OH scavenger, which is expected to increase the SOA yield and counteract the density effect. Also the simulation contains enough water vapour to scavenge stabilised Criegee intermediates.

In this model as well as in other models recently developed to predict SOA yields (Cocker et al., 2001; Kamens and Jaoui, 2001; Bian and Bowman, 2002), a wide variety of gas-phase reaction products are lumped on the basis of their vapour pressures, and representative  $\alpha_i$ ,  $K_{om,i}$  and  $B_i$  values are calculated for each lumped species.  $K_{om,i}$  values calculated on the basis of atmospheric gas phase chemistry mechanisms are generally much lower than the  $K_{om,i}$  values obtained by fitting to SOA measurements, which have been attributed to association reactions of organics in the aerosol phase (Tobias and Ziemann, 2000; Kamens and Jaoui, 2001). Accordingly, Jenkin (2004) applied a scaling factor of 120 to the  $K_{om,i}$  values calculated for SOA formation from  $\beta$ -pinene ozonolysis. The stoichiometric yields  $\alpha_i$  are assumed to be independent of temperature, whereas the gas-particle partitioning coefficients  $K_{om,i}$  are assumed to have a Clausius-Clapeyron-type temperature dependence due to the dependence on vapour pressure as described in Sect. 2.6. As a consequence of this the two-product model usually implies proportionality between SOA yield and inverse temperature.

### 3 Results and discussion

SOA formation experiments have been performed at six different temperatures in the range of 263 K–303 K under dry and humid conditions and SOA yields have been determined from the measured number size distributions and calculated amounts of reacted  $\beta$ -pinene as detailed in Sect. 2. The conditions and results of the individual experiments are listed in Tables 1 and 2.

#### 3.1 Particle concentrations and size distributions

Figure 2 displays exemplary particle number and volume size distributions of dry experiments performed with about 1.25 ppmv ozone and 1.28–1.37 ppmv  $\beta$ -pinene, except for the measurement at 293 K performed with 1.61 ppmv  $\beta$ -pinene. The modal diameter of the number size distributions was fairly constant (20 nm–30 nm), and the integrated

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number concentrations exhibited a trend to decrease with decreasing temperature. In contrast, the modal diameter of the volume size distributions is 30 nm at 283 K–303 K but increases over 38 nm at 278 K to 60 nm at 263 K and 273 K. The integrated volume concentrations exhibited an increasing trend with decreasing temperature (albeit oscillatory rather than monotonous, as discussed below).

Figure 3 displays exemplary particle number and volume size distributions of humid experiments (26%–68% RH) with about 1.25 ppmv ozone and 0.97–1.76 ppmv  $\beta$ -pinene. Under these conditions, both the modal diameter of the number size distributions (20 nm–40 nm) and the integrated particle number concentrations decreased with decreasing temperature. The integrated volume concentration also exhibited a clear decrease with decreasing temperature, whereas the modal diameters of the volume size distributions increased (40 nm–60 nm). Compared to the dry experiments, the particle number concentrations under humid conditions were generally lower, whereas the particle volume concentrations were higher at high temperatures (283 K–293 K) and lower at low temperatures (263 K–273 K).

Overall, the measured particle concentrations and size distributions indicate that the yield of nucleating species responsible for new particle formation decreased with decreasing temperature, both under dry and humid conditions. Under humid conditions also the yield of condensing species responsible for particle growth decreased with decreasing temperature. For all temperatures the addition of water vapour resulted in a reduction of the yield of nucleating species, whereas the yield of condensing species was reduced at low temperatures (263 K and 273 K) and increased at high temperatures (283 K and 293 K).

### 3.2 Concentration dependence of SOA yield

Figure 4 summarises the results of all dry experiments in a plot of SOA yield versus  $M_o$ . At all temperatures, the yield exhibits a near-linear increase with  $M_o$  for  $M_o < 10 \mu\text{g m}^{-3}$  and reaches a near-constant maximum level for  $M_o > 100 \mu\text{g m}^{-3}$ . This behaviour can

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be fitted with the two-product model outlined in Sects. 2.5 and 2.6; the parameters of the shown fit lines are summarized in Table 5 and will be discussed below.

The error bars depict the standard deviations for  $M_o$  and SOA yield, calculated as described in Sect. 2.4. They illustrate that the relative standard deviations of repeated measurements within one experiment were mostly 10% or less. The standard deviations between the mean values of SOA yield obtained in different experiments repeated under near-identical conditions (similar  $T$  and  $\Delta[\beta\text{-pinene}]$ ) were generally  $\leq 0.05$ , corresponding to relative standard deviations up to 15%.

The standard deviation of the ozonolysis reaction rate coefficient  $k_{O_3}$  ( $s_{k_{O_3}}$ ) was not included in the error bars of Fig. 4, i.e.  $s_{k_{O_3}}$  was excluded from their calculation through Eq. (9).  $s_{k_{O_3}}$  varies only little over the investigated temperature range and does not affect the statistical uncertainty of our experimental data. It should, however, be taken into account when comparing the results to other studies and extrapolating to the atmosphere. When  $s_{k_{O_3}}$  is included in Eq. (9),  $s_Y$  is a factor of 2 to 3 larger than the error bars displayed in Fig. 4. The same applies to the SOA yields and uncertainties of the humid experiments presented below (Sect. 2.4, Fig. 5). Clearly, a reduction of the uncertainty of the ozonolysis rate coefficient is of central importance for reducing uncertainties of SOA formation and mass concentrations in atmospheric models. If future investigations were to reveal differences between the actual value of  $k_{O_3}$  and the value used here, the results of this study could be scaled accordingly.

As illustrated in Fig. 4, the maximum yield from the study by Hoffmann et al. (1997) at 292 K (open diamonds) agrees quite well with the maximum yield from our study at 293 K (filled diamonds). At  $M_o < 150 \mu\text{g m}^{-3}$ , however, the yields of Hoffmann et al. (1997) were about 20% higher, even though they had assumed lower particle density (1.0 vs.  $1.2 \text{ g cm}^{-3}$ , Sect. 2.7). A possible explanation for the differences is that the denominator in the calculation of the SOA yield,  $-\Delta[\beta\text{-pinene}]$ , was measured by Hoffmann et al. (1997) whereas it has been calculated in this study, subject to the large uncertainty of  $k_{O_3}$  outlined above. Moreover, the SOA particles in our flow tube experiments were freshly formed, whereas chemical aging over multiple hours may have

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played a role in the chamber experiments of Hoffmann et al. (1997).

Unexpectedly, the SOA yields measured under dry conditions did not exhibit a monotonous increase with decreasing temperature. Even when the statistical uncertainties of the measurement results are taken into account, the yields observed at 263 K were generally lower than those at 273 K and 278 K (most evident at  $M_o > 30 \mu\text{g}/\text{m}^3$ ; Fig. 4) and the yields observed at 283 K were lower than those at 263 K and 293 K (Fig. 3). This complex, non-linear behaviour will be discussed below.

Figure 5 illustrates the concentration dependence of SOA yields observed under humid conditions. It is qualitatively similar to the concentration dependence exhibited by the dry experiments and can also be fitted with the two-product model outlined in Sects. 2.5 and 2.6; the parameters of the shown fit lines are summarized in Table 6 and will be discussed below.

Compared to the dry experiments, the maximum yields decreased by  $\sim 35\%$  at low temperatures (263 K–273 K) but they increased by  $\sim 80\%$  at 283 K and by  $\sim 30\%$  at 293 K, respectively. The yields reported by Griffin et al. (1999) for  $M_o < 30 \mu\text{g}/\text{m}^3$  at 307 K–308 K (Fig. 5, open triangles) are by more than a factor of 5 lower than the ones observed in our experiments at 293 K, but their two-product model fit predicts a maximum yield comparable to our study (0.511 vs. 0.436). The difference might be due to the use of an OH scavenger (2-butanol) in the experiments of Griffin et al. (1999).

In contrast to the irregular and weak increase of SOA yield with decreasing temperature observed under dry conditions, the humid experiments exhibited a pronounced monotonous decrease of yield with decreasing temperature as detailed below.

### 3.3 Temperature dependence of SOA yield

Figure 6 illustrates the temperature dependence of SOA yields at  $M_o = 10 \mu\text{g}/\text{m}^3$  (a) and  $M_o = 250 \mu\text{g}/\text{m}^3$  (b) as observed and modelled in our study and other investigations of SOA formation from ozonolysis of  $\beta$ -pinene.  $M_o = 10 \mu\text{g}/\text{m}^3$  was chosen as an exemplary atmospheric particle mass concentration level.  $M_o = 250 \mu\text{g}/\text{m}^3$  is well

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above typical atmospheric aerosol loadings, but it was chosen for robust comparison of measured and modelled maximum yields, because it is well in the saturation range (near-constant maximum level of SOA yield). As illustrated in Figs. 4 and 5, the relations and conclusions obtained by comparison of effective maximum SOA yields at  $250 \mu\text{g m}^{-3}$  are generally also valid for concentration levels at the lower end of the saturation range, i.e. around  $100 \mu\text{g m}^{-3}$ , which are relevant for polluted environments.

Under dry conditions the results of our and other experiments are consistent with an overall trend of increasing SOA yield with decreasing temperature, as predicted by the two-product model of Jenkin (2004), which is based on the lumping of species from a detailed mechanism of gas phase chemistry (Sect. 2.7.2). When a linear fit is applied to our data plotted against inverse  $T$  (dashed red lines in Fig. 6), the slopes are of similar magnitude as predicted by Jenkin (2004). At  $M_o=10 \mu\text{g m}^{-3}$  the fit to the measurement data is  $\sim 50\%$  steeper than the model prediction by Jenkin (2004) (277 K vs. 186 K); at  $M_o=250 \mu\text{g m}^{-3}$  it is  $\sim 40\%$  less steep (108 K vs. 179 K). The steeper slope at lower particle mass concentration (277 K vs. 108 K) is consistent with the two-product model predicting that for lower temperatures the maximum yield should be reached at lower  $M_o$ .

However, the measured yields exhibit substantial oscillatory deviations from the predicted linear increase with  $1/T$ . The largest oscillatory variations occurred at 278 K–283 K, where the SOA yield increased by a factor of  $\sim 2$  for a temperature change of 5 K.

At  $M_o=10 \mu\text{g m}^{-3}$  and in the temperature range of 292 K–308 K our dry measurement data agree to within 18% with the model results of Jenkin (2004) and the measurement of Yu et al. (1999) (306 K), whereas the yields of Hoffmann et al. (1997) are 43% higher. At 273 K–283 K our dry data deviate by up to 49% from the model of Jenkin (2004) (lower at 283 K, higher at 273 and 278 K), whereas at 263 K they agree again to within 7%. At  $M_o=250 \mu\text{g m}^{-3}$  our dry data at 303 K, 283 K, and 263 K agree to within 14% with the model of Jenkin (2004). At 293 K our dry data agree well with those of Hoffmann et al. (1997) which are 48% higher than the model results. At 278 K and

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273 K our dry data are also 40%–51% higher than the model results by Jenkin (2004).

Under humid conditions our measurement data exhibit a linear decrease with inverse temperature, which is opposite to the model temperature dependence of Jenkin (2004). The slope of a linear fit to the data is much less steep at  $M_o=10 \mu\text{g m}^{-3}$  (–44 K) than at  $M_o=250 \mu\text{g m}^{-3}$  (–620 K). At both concentration levels the fit lines intercept the model line of Jenkin (2004) at 273 K.

At  $M_o=10 \mu\text{g m}^{-3}$  and 273 K our humid measurement data agree to within 16% with the model of Jenkin (2004); at 263 K the model prediction is 29% higher, at 293 K it is 46% lower. The yield found by Griffin et al. (1999) at 308 K was 63% lower than the model prediction. At  $M_o=250 \mu\text{g m}^{-3}$  our humid data at 273 K agree to within 9% with the model of Jenkin (2004); at 263 K our data are 39% lower and at 293 K they are 79% higher than the model predictions. The two-product model extrapolations based on the measurements of Griffin et al. (1999) agree to within 12% with the model of Jenkin (2004). The yield reported by Lee et al. (2006) is 26% lower than the model prediction by Jenkin (2004) and 58% lower than our measured yield.  $M_o$  was only  $174 \mu\text{g m}^{-3}$  in the experiment of Lee et al. (2006), but according to our results this should already be in the saturation range with very similar yields as at  $M_o=250 \mu\text{g m}^{-3}$ . The yield at 290 K–285 K reported by Jaoui and Kamens (2003) agree to within 4% with the model of Jenkin (2004).

The negative dependence on inverse temperature observed under humid conditions indicates that the SOA yield is governed much more by the temperature and humidity dependence of the involved chemical reactions than by vapour pressure temperature dependencies, which are always positive. The major differences between the results of dry and humid experiments (oscillatory positive vs. linear negative dependence on  $1/T$ ; up to 50% variation of  $Y$  at identical  $T$ ) indicate that the abundance of water vapour may actually have a stronger influence on SOA formation than temperature. Because the humid experiments in this study have been conducted at a fairly uniform level of relative humidity (~50%), the actual water vapour concentrations in the reactor were steeply increasing with temperature (from 0.1% v/v at 263 K to 1.6% v/v at 293 K).

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Thus further experiments will be required for unambiguous distinction of temperature and humidity effects on the reaction pathways of SOA formation. However, in areas with vegetation (where monoterpenes are emitted) the concentration of water vapour is mainly controlled by temperature. E.g. we experience dew-fall, when the sun sets and the air cools down. For comparison the saturation concentration of water vapour changes from 0.28% v/v at 263 K to 2.32% v/v at 293 K. Thus these first experiments can give a good indication of the effect of temperature on atmospheric SOA yield under humid conditions. In any case, the strong influence of water vapour observed in our experiments indicates that different results from different studies of SOA formation (Fig. 6b) may well be due to changes in the involved chemical reactions caused by varying abundances of water vapour or other chemical components of the reaction mixture, such as OH scavengers. Moreover, the oscillatory temperature dependence observed in our dry experiments indicates that under certain conditions large changes of SOA yield can be caused by small temperature variations.

For the atmospherically relevant concentration level and temperature range of  $M_o=10\ \mu\text{g m}^{-3}$  and 263 K–293 K, the measurement and model results of this and earlier studies displayed in Fig. 6a indicate that the SOA yield of  $\beta$ -pinene ozonolysis may be well represented by an average value of 0.15 with an uncertainty estimate of  $\pm 0.05$ . This uncertainty range comprises the results of all humid and most dry experiments of this and earlier studies as well as the model results of Jenkin (2004). If the small temperature dependence observed under humid conditions can be extrapolated, the average value and uncertainty range of  $0.15\pm 0.05$  may be extendable over a temperature range as wide as 250 K–330 K.

### 3.4 Two-product model fit results

Clearly, the two-product model approach is a gross simplification of the complex reaction mechanisms and multiphase processes leading to SOA formation. Nevertheless, this approach is routinely used for the modelling of SOA formation in both process studies and atmospheric models. Therefore we have fitted our measurement data with

the two-product model, using two alternative fitting procedures as detailed in Sect. 2.6 (“B fit” and “free fit”).

When constraining the temperature dependence of the partitioning coefficients by Eq. (11) with  $B_1=6153\text{ K}$  and  $B_2=5032\text{ K}$  and fitting the complete data set including all temperature levels at once (“B fit”), we obtained the results summarized in Tables 5 and 6.

Under dry conditions (Table 5), the best-fit partitioning coefficients at 303 K were  $K_{om,1,303\text{ K}}=0.038\text{ m}^3\mu\text{g}^{-1}$  and  $K_{om,2,303\text{ K}}=0.001\text{ m}^3\mu\text{g}^{-1}$ ; the  $K_{om,i}$  values at other temperatures follow the trend prescribed by Eq. (11). The stoichiometric yields exhibited temperature dependent oscillations comparable to the oscillations of the SOA yield. At all temperatures except 283 K, the stoichiometric yield of low volatile products ( $\alpha_1$ : 0.14–0.30) was larger than that of semi-volatile products ( $\alpha_2$ : 0–0.25).

Under humid conditions (Table 6), the best fit values of  $K_{om,1}$  were by a factor of 0.8 lower and those of  $K_{om,2}$  were by a factor of 5 higher than under dry conditions, indicating lower effective volatility of the lumped semi-volatile products under humid conditions. The stoichiometric yield of low-volatile products exhibited a steep increase with temperature ( $\alpha_1$ : 0.15–0.44), corresponding to the increase of SOA yield. The stoichiometric yield of semi-volatile products exhibited no pronounced trend and was generally lower than under dry conditions ( $\alpha_2$ : 0.001–0.1).

When fitting the data set obtained at each temperature independently (“free fit”), we obtained the results summarized in Tables 7 and 8.

Under dry conditions (Table 7), the best-fit partitioning coefficient of the lumped low-volatile products exhibited oscillatory increase with decreasing temperature ( $K_{om,1}$ :  $0.04\text{ m}^3\mu\text{g}^{-1}$ – $64\,000\text{ m}^3\mu\text{g}^{-1}$ ), whereas the partitioning coefficient of the semi-volatile products exhibited no pronounced trend and was nearly as high as that of the low-volatile species at 273 K and 303 K ( $K_{om,2}$ : 0.001–0.13  $\text{m}^3\mu\text{g}^{-1}$ ). The stoichiometric yield of low-volatile products exhibited temperature dependent oscillations comparable to the oscillations of the SOA yield ( $\alpha_1$ : 0.12 - 0.39), and at most temperatures except 278 K and 303 K it was larger than the stoichiometric yield of semi-volatile prod-

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ucts ( $\alpha_2$ : 0.002–0.29), which was inversely correlated to the oscillations of  $\alpha_1$  and SOA yield.

Under humid conditions (Table 6), the best fit values of  $K_{om,1}$  exhibited a pronounced monotonous increase with decreasing temperature (0.06–203 m<sup>3</sup>  $\mu$ g<sup>-1</sup>), whereas  $K_{om,2}$  exhibited no pronounced trend and was nearly as high as that of the low-volatile species at 273 K and 293 K (0.06–0.23 m<sup>3</sup>  $\mu$ g<sup>-1</sup>).  $\alpha_1$  exhibited an oscillatory increase with temperature ( $\alpha_1$ : 0.06 - 0.32), and  $\alpha_2$  exhibited inversely correlated oscillations of similar magnitude ( $\alpha_2$ : 0.06–0.32).

The increase of  $\alpha_1$  with increasing temperature observed under humid conditions is consistent with the increase of the yield of nucleating species inferred above from the measured particle concentrations and size distributions (Sect. 3.1). The other trends and implications of the particle concentration and size distribution measurements, however, are not directly reflected by the two-product model fit parameters. Obviously, the lumped low-volatile products cannot be readily interpreted as nucleating species that lead to new particle formation, and the lumped semi-volatile products cannot be readily interpreted as condensing species.

Overall, the differences between the results obtained with different fitting procedures and the oscillatory behaviour of the fit parameters indicate that indeed the two-product model is insufficient for a mechanistic description and reliable extrapolation of the temperature and humidity dependence of SOA formation. In view of the wide use of the two-product model and in view of the lack of readily available and efficient alternatives, however, possible mechanistic interpretations and implications of the fit parameters will be discussed below.

### 3.5 Mechanistic implications of two-product model fit parameters

As noted in Sect. 2.7 and as illustrated in Fig. 6, the two-product model by Jenkin (2004) exhibits a linear positive dependence of SOA yield on inverse temperature. The linear dependence is a consequence of assigning a Clausius-Clapeyron-type temperature dependence to the gas-particle partitioning coefficients  $K_{om,i}$  (Sect. 2.6, Eq. 11)

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and assuming no temperature dependence of the stoichiometric yields  $\alpha_j$ . To reproduce the oscillations of the SOA yields under dry conditions and the negative temperature dependence under humid conditions with the two-product model, however, it is necessary to allow a temperature dependence of  $\alpha_j$ , i.e. variations of the yields of low-volatile and semi-volatile reaction products with temperature. This implies a change in product yields, i.e. the amounts of low-volatile and semi-volatile species produced, with temperature.

The formation of condensable species from volatile precursor gases involve numerous reaction steps and intermediates (Jenkin, 2004), and a combination of exothermal and endothermal processes may well lead to complex temperature dependencies as observed in our dry experiments. Contrary to gas-particle partitioning, which is expected to decrease the SOA yield with increasing temperature (decrease of  $K_{om,i}$  with increasing T), the chemical reactions leading to second-generation products with lower volatility are likely to be accelerated at higher temperatures.

Differences in the temperature dependency of competing reaction pathways may lead to changes of the real reaction product distribution and thus to changes of the effective properties of the lumped low-volatile and semi-volatile model products (Bian and Bowman, 2005). Under these conditions, the temperature-normalized gas-particle partitioning coefficients,  $K_{om,i}/T$ , are likely to exhibit deviations from the exponential dependence on inverse temperature, which is expected for constant product composition according to Eq. (11). In other words, deviations from a linear dependence of the logarithm of  $K_{om,i}/T$  on  $1/T$  indicate changes in the chemical composition of the reaction products.

In Fig. 7 the temperature-normalized partitioning coefficients,  $K_{om,i}/T$ , obtained from the different fits (“B fit” and “free fit”) to the dry and humid data set are plotted on a logarithmic scale against  $1/T$  on a linear scale. The  $K_{om,i}/T$  values obtained from “B fits” exhibit a linear dependence on  $1/T$  as prescribed by Eq. (11).  $K_{om,1}/T$  was practically the same under dry and humid conditions, whereas  $K_{om,2}/T$  was by a factor of 5 higher under humid conditions, indicating a strong influence of humidity on the

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gas-particle partitioning of semi-volatile products.

Among the  $K_{om,i}/T$  values obtained by “free fits”, only the  $K_{om,2}/T$  values from the humid data set exhibit a near-linear dependence on  $1/T$ , indicating fairly constant properties and composition of semi-volatile products. The dry  $K_{om,2}/T$  values and the  $K_{om,1}/T$  exhibit substantial deviations from linearity, indicating changes of reaction product composition. From 273 K to 263 K the  $K_{om,1}/T$  exhibits a particularly pronounced increase, which is by several orders of magnitude higher than expected from the near-linear dependence observed at higher temperatures. It is tempting to speculate that this increase might be related to the freezing of water, but it is actually more pronounced under dry conditions and thus most likely due to effects of temperature on the chemical reaction mechanism and product distribution.

In any case, Fig. 7 reconfirms that the two-product model is insufficient for a mechanistic description of the temperature dependence of SOA formation. It demonstrates a need for further systematic investigations and mechanistic elucidation of the complex physico-chemical processes involved in atmospheric particle formation and gas-particle interactions (multiphase chemical reactions, mass transport, and phase transitions (Pöschl et al., 2005; Fuzzi et al., 2006)).

## 4 Conclusions

Our investigations of SOA formation from the ozonolysis of  $\beta$ -pinene demonstrated that not only the partitioning coefficients of the reaction products but also the relative contributions of different gas-phase or multiphase reaction pathways are dependent on temperature and humidity. Under humid conditions the SOA yield was actually found to increase rather than decrease with increasing temperature, indicating that the temperature and humidity dependence of chemical reactions is more important than the temperature dependence of vapour pressures.

Further investigations are needed for mechanistic elucidation and reliable description of the complex physico-chemical processes involved in SOA formation, and the

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influence of temperature and humidity should be considered both for gas-particle partitioning of VOC oxidation products and for the pathways and kinetics of gas phase and multiphase chemical reactions.

In atmospheric models both the temperature of oxidative processing and the local temperature of gas-particle partitioning should be taken into account for the modelling of SOA. Differences between these temperatures and their effects could be particularly important in the tropics, where high BVOC emissions and high oxidizing capacities under humid conditions can lead to large amounts of SOA, which by deep convection can be rapidly transported to high altitudes where low temperatures favour further condensation.

*Acknowledgements.* The authors would like to thank G. Schuster for his technical expertise and support of the experimental work. Thanks to B. Svensmark, T. Hoffmann and J. Curtius for helpful discussions. The project was funded by the Max Planck Society. O. J. Nielsen and M. Bilde acknowledge financial support from the Danish Natural Science Research Council.

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**Table 1.** Conditions and results of individual dry experiments:  $-\Delta[\beta\text{-pinene}]$  = decrease of  $\beta$ -pinene mass concentration,  $N$  = total particle number concentration,  $M_o$  = total particle mass concentration,  $s_{M_o}$  = standard deviation of  $M_o$ ,  $Y$  = SOA yield,  $s_Y$  = standard deviation of  $Y$ ,  $n$  = number of measured number size distributions in each experiment, Sheath = sheath air flow in the DMA, reaction time ( $\Delta t$ ) = 40 s.

	$T$ K	$[\beta\text{-pinene}]_0$ ppbv	$[\text{ozone}]_0$ ppbv	$-\Delta[\beta\text{-pinene}]$ $\mu\text{g m}^{-3}$	$N$ # $\text{cm}^{-3}$	$M_o$ $\mu\text{g m}^{-3}$	$s_{M_o}$ $\mu\text{g m}^{-3}$	$Y$	$s_Y$	$n$	Sheath $\text{l min}^{-1}$
bp240106.6	263	601	1031	49.5	5.5E+05	9.3	0.48	0.19	0.02	5	3.0
bp240106.5	263	601	1362	65.2	7.5E+05	12.6	0.74	0.19	0.02	11	3.0
bp240106.4	263	754	1937	116.2	1.3E+06	27.2	1.59	0.23	0.02	12	3.0
bp100106.3	263	2893	623	142.6	1.9E+06	30.9	2.17	0.22	0.02	11	9.7
bp240106.3	263	3024	1934	462.6	3.3E+06	123.9	5.80	0.27	0.02	5	3.0
bp240106.1	263	3031	1964	470.8	3.1E+06	120.8	6.44	0.26	0.02	23	3.0
bp100106.2	263	5705	1126	501.7	3.4E+06	121.0	8.27	0.24	0.02	15	9.7
bp240106.2	263	5977	1991	928.5	4.4E+06	245.6	7.35	0.26	0.02	9	3.0
bp170106.3	273	754	669	44.9	3.4E+05	10.1	0.56	0.23	0.02	13	9.7
bp170106.4	273	754	1190	79.6	9.7E+05	23.8	1.74	0.30	0.03	13	6.0
bp040106.2	273	5991	376	194.6	2.5E+06	60.6	3.11	0.31	0.02	9	9.7
bp170106.5	273	3151	1182	326.7	3.9E+06	120.7	8.48	0.37	0.03	12	6.0
bp170106.2	273	6204	1188	635.8	4.2E+06	241.3	7.81	0.38	0.03	11	9.7
bp220506.5	278	599	545	30.5	4.2E+05	6.0	0.51	0.20	0.02	7	9.7
bp220506.2	278	783	721	52.7	7.5E+05	10.6	1.13	0.20	0.02	22	9.7
bp220506.1	278	1375	1249	159.6	2.3E+06	44.1	4.75	0.28	0.03	24	9.7
bp220506.4	278	2003	1815	336.9	4.1E+06	114.6	11.90	0.34	0.04	15	9.7
bp220506.3	278	2782	2380	611.0	5.1E+06	238.9	18.49	0.39	0.04	20	9.7
bp270106.1	283	1565	437	66.6	4.5E+05	2.0	0.04	0.03	0.00	10	3.0
bp150306.1	283	1500	651	95.1	1.2E+06	7.2	0.06	0.08	0.00	12	9.7
bp150306.2a	283	1506	797	116.8	1.9E+06	11.5	0.07	0.10	0.01	11	9.7
bp160306.1a	283	1363	1266	168.2	2.7E+06	25.2	0.29	0.15	0.01	17	9.7
bp270106.2	283	1565	1262	192.3	2.4E+06	21.7	0.38	0.11	0.01	16	3.0
bp230106.6	283	1630	2086	329.9	3.6E+06	52.7	0.70	0.16	0.01	12	3.0
bp230106.5	283	3253	2073	649.3	5.2E+06	124.4	0.80	0.19	0.01	10	3.0
bp230106.1	283	6431	1233	748.8	4.8E+06	124.6	1.38	0.17	0.01	13	9.7
bp230106.3	283	6430	1254	761.5	5.5E+06	143.7	1.56	0.19	0.01	8	3.0
bp230106.2	283	6432	1288	782.3	5.1E+06	147.8	2.01	0.19	0.01	11	9.7
bp230106.4	283	6430	2097	1273.1	6.6E+06	280.1	1.76	0.22	0.01	9	3.0
bp140106.3	293	774	1280	105.3	2.2E+06	15.9	0.54	0.15	0.01	4	9.7
bp191205.4	293	5444	199	111.9	2.4E+06	20.5	0.26	0.18	0.01	10	5.0
bp130106.1	293	1611	658	112.4	2.6E+06	23.6	0.17	0.21	0.01	11	9.7
bp140106.1	293	1611	1255	214.4	3.7E+06	56.9	0.79	0.27	0.02	10	9.7
bp191205.1	293	5443	415	233.1	3.5E+06	53.8	0.78	0.23	0.01	10	5.0
bp191205.2	293	5453	793	446.1	4.7E+06	131.3	1.65	0.29	0.02	10	5.0
bp140106.2	293	6364	1269	828.4	5.8E+06	283.6	3.23	0.34	0.02	4	9.7
bp191205.3	293	10863	790	853.2	5.7E+06	274.9	3.45	0.32	0.02	8	5.0
bp210306.2	303	851	1309	128.0	1.1E+06	7.4	0.16	0.06	0.00	17	9.7
bp201205.2	303	6682	215	158.0	1.6E+06	15.9	0.50	0.10	0.01	8	9.7
bp210306.1	303	1361	1261	197.1	2.7E+06	37.0	0.82	0.19	0.01	16	9.7
bp201205.3	303	6671	431	316.8	3.4E+06	64.0	0.82	0.20	0.01	22	9.7
bp201205.1	303	6677	846	622.2	4.3E+06	135.3	2.54	0.22	0.01	8	9.7
bp201205.4	303	10014	842	905.9	5.0E+06	205.2	4.21	0.23	0.01	10	9.7

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**Table 2.** Conditions and results of individual humid experiments:  $-\Delta[\beta\text{-pinene}]$  = decrease of  $\beta$ -pinene mass concentration,  $N$  = total particle number concentration,  $M_{o,\text{humid}}$  = total particle mass concentration not corrected for hygroscopic growth,  $s_{M_{o,\text{humid}}}$  = standard deviation of  $M_{o,\text{humid}}$ ,  $Y$  = SOA yield corrected for hygroscopic growth,  $s_Y$  = standard deviation of  $Y$ ,  $n$  = number of measured number size distributions in each experiment,  $RH$  = relative humidity,  $GF$  = growth factor, sheath air flow in the DMA =  $9.7 \text{ l min}^{-1}$ , reaction time ( $\Delta t$ ) = 40 s.

	$T$ K	$[\beta\text{-pinene}]_0$ ppbv	$[\text{ozone}]_0$ ppbv	$-\Delta[\beta\text{-pinene}]$ ( $\mu\text{g/m}^3$ )	$N$ ( $\#\text{/cm}^3$ )	$M_{o,\text{humid}}$ ( $\mu\text{g/m}^3$ )	$s_{M_{o,\text{humid}}}$ ( $\mu\text{g/m}^3$ )	$Y$	$s_Y$	$n$	$RH$ %	$GF$
020606_3	263	669	614	32.9	$1.6\text{E}+05$	3.5	0.18	0.10	0.009	13	34	1.01
020606_2	263	966	900	69.4	$4.5\text{E}+05$	9.9	0.44	0.14	0.010	17	43	1.01
020606_1	263	1997	1747	277.4	$1.8\text{E}+06$	49.3	1.77	0.17	0.013	12	37	1.01
020606_4	263	3760	3022	895.9	$3.5\text{E}+06$	164.2	5.26	0.18	0.012	13	34	1.01
070606_1	273	561	490	21.6	$9.8\text{E}+04$	1.9	0.12	0.08	0.007	10	26	1.01
240506_3	273	817	657	47.7	$3.2\text{E}+05$	8.7	0.44	0.17	0.043	14	55	1.02
240506_1	273	1460	1249	161.5	$4.6\text{E}+05$	26.8	2.13	0.16	0.042	13	35	1.01
240506_2	273	2116	1734	323.8	$2.0\text{E}+06$	85.9	3.39	0.25	0.063	18	46	1.02
070606_2	273	2571	2583	584.7	$1.9\text{E}+06$	145.6	2.72	0.24	0.016	9	28	1.01
060606_2	283	1363	1266	168.2	$1.8\text{E}+06$	52.3	3.53	0.29	0.027	13	50	1.02
060606_1	283	2550	2654	654.6	$3.0\text{E}+06$	257.8	14.54	0.37	0.031	22	57	1.02
230506_4	293	524	805	44.9	$2.4\text{E}+05$	2.1	0.30	0.04	0.012	9	64	1.03
230506_2	293	785	1293	107.8	$1.0\text{E}+06$	32.9	0.55	0.28	0.068	9	61	1.03
230506_5	293	1019	807	87.6	$8.2\text{E}+05$	25.3	0.53	0.26	0.063	9	68	1.04
230506_1	293	1759	1256	234.0	$1.6\text{E}+06$	70.1	1.39	0.27	0.066	23	63	1.03
230506_3	293	2114	1835	409.9	$2.8\text{E}+06$	176.8	3.84	0.40	0.095	10	63	1.03

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**Table 3.** Start values for the two-product model fit to the measurement data from dry and humid experiments:  $\alpha_1$  and  $\alpha_2$  are the stoichiometric yields of the low volatile and semi volatile species.

T (K)	dry		humid	
	$\alpha_1$	$\alpha_2$	$\alpha_1$	$\alpha_2$
263	0.10	0.17	0.15	0.04
273	0.09	0.29	0.25	0.04
278	0.10	0.30		
283	0.03	0.18	0.26	0.13
293	0.01	0.33	0.40	0.04
303	0.08	0.16		

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**Table 4.** Experimental conditions for studies regarding yield from  $\beta$ -pinene ozonolysis.

	T (K)	Seed aerosol	RH (%)	OH scavenger
Hoffmann et al. (1997)	292	+	–	–
Griffin et al. (1999)	307–308	+	5	2-butanol
Yu et al. (1999)	306–308	+	–	2-butanol
Jaoui and Kamens (2003)	285–290	–	40–50	–
Lee et al. (2006)	293	+	6.3	cyclohexane
This study	263–303	–	<0.03; 26–68	–

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**Table 5.** Best-fit values of the two-product model B fits (Sect. 2.6) to the dry data from our study and the fit parameters from Hoffmann et al. (1997)<sup>a</sup> (292 K) (one-product model, Fig. 4).  $K_{om,i}$  = partitioning coefficient,  $\alpha_i$  = stoichiometric yield,  $S_T$  = optimised residual parameter, n = number of data points (experiments).

T (K)	$K_{om,1}(\text{m}^3\mu\text{g}^{-1})$	$K_{om,2}(\text{m}^3\mu\text{g}^{-1})$	$\alpha_1$	$\alpha_2$	$S_T$	n
263	0.724	0.011	0.207	0.080	2.75	8
273	0.319	0.006	0.284	0.173	1.73	5
278	0.217	0.004	0.274	0.248	2.11	5
283	0.149	0.003	0.139	0.184	9.30	11
293	0.073	0.002	0.297	0.136	3.22	8
303	0.038	0.001	0.264	0	4.87	6
292 <sup>a</sup>	0.11	–	0.35	–		

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**Table 6.** Best-fit values of the two-product model “B fits” (Sect. 2.6) to the humid data from our study and the fit parameters from Griffin et al. (1999)<sup>b</sup> (308 K) (two-product model, Fig. 5).  $K_{om,i}$  = partitioning coefficient,  $\alpha_i$  = stoichiometric yield,  $S_T$  = optimised residual parameter, n = number of data points (experiments).

T (K)	$K_{om,1}$ ( $\text{m}^3 \mu\text{g}^{-1}$ )	$K_{om,2}$ ( $\text{m}^3 \mu\text{g}^{-1}$ )	$\alpha_1$	$\alpha_2$	$S_T$	n
263	0.590	0.054	0.148	0.036	0.41	4
273	0.260	0.028	0.229	0.026	4.67	5
283	0.122	0.015	0.286	0.115	1.08E-06	2
293	0.060	0.009	0.435	0.001	4.79	5
308 <sup>b</sup>	0.195	0.003	0.026	0.485		

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**Table 7.** Best-fit values of the two-product model “free fits” (Sect. 2.6) to dry data from our study.  $K_{om,i}$  = partitioning coefficient,  $\alpha_i$  = stoichiometric yield,  $S_T$  = optimised residual parameter, n = number of data points (experiments).

T (K)	$K_{om,1}(\text{m}^3\mu\text{g}^{-1})$	$K_{om,2}(\text{m}^3\mu\text{g}^{-1})$	$\alpha_1$	$\alpha_2$	$S_T$	n
263	63950	0.037	0.157	0.119	2.51	8
273	0.135	0.130	0.389	0.002	1.55	5
278	3.017	0.009	0.193	0.290	0.53	5
283	0.098	0.001	0.181	0.158	7.07	11
293	0.067	0.001	0.313	0.119	3.18	8
303	0.041	0.040	0.118	0.139	4.60	6

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**Table 8.** Best-fit values of the two-product model “free fits” (Sect. 2.6) to the humid data from our study.  $K_{om,i}$  = partitioning coefficient,  $\alpha_i$  = stoichiometric yield,  $S_T$  = optimised residual parameter,  $n$  = number of data points (experiments).

T (K)	$K_{om,1}(\text{m}^3\mu\text{g}^{-1})$	$K_{om,2}(\text{m}^3\mu\text{g}^{-1})$	$\alpha_1$	$\alpha_2$	$S_T$	$n$
263	203	0.184	0.056	0.127	0.20	4
273	0.233	0.232	0.196	0.055	4.59	5
283	0.185	0.050	0.078	0.315	$1.8 \cdot 10^{-08}$	2
293	0.060	0.059	0.315	0.121	4.78	5

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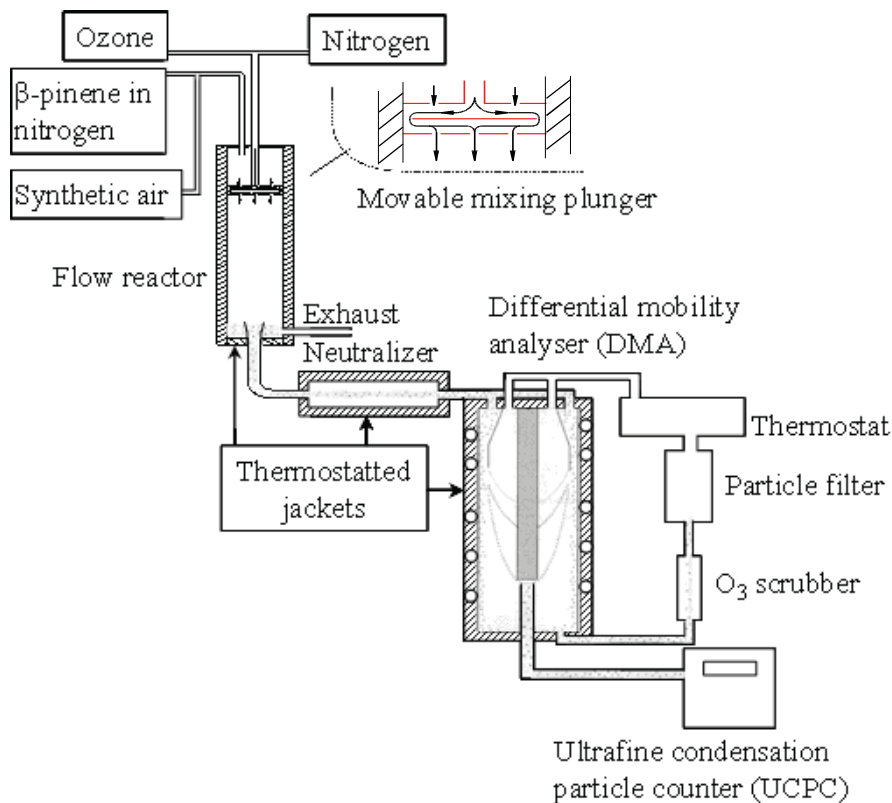
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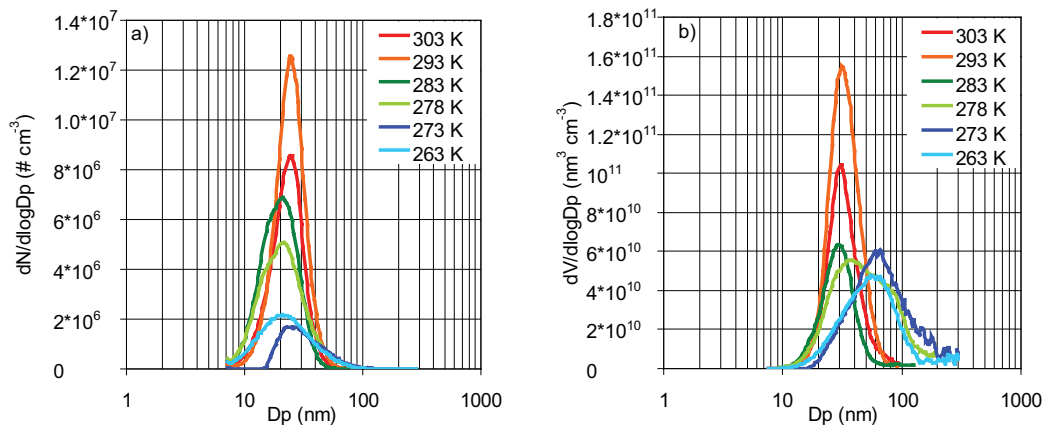
**Temperature and humidity dependence of SOA yield**

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**Fig. 1.** Schematic drawing of the experimental set-up.[Title Page](#)[Abstract](#)[Introduction](#)[Conclusions](#)[References](#)[Tables](#)[Figures](#)[◀](#)[▶](#)[◀](#)[▶](#)[Back](#)[Close](#)[Full Screen / Esc](#)[Printer-friendly Version](#)[Interactive Discussion](#)

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**Fig. 2.** Particle number (a) and volume (b) size distributions from dry experiments with  $[\beta\text{-pinene}]_0=1.28\text{ ppmv}-1.37\text{ ppmv}$  (except for 293 K:  $[\beta\text{-pinene}]_0=1.61\text{ ppmv}$ ) and  $[\text{O}_3]_0 \approx 1.25\text{ ppmv}$  at different temperatures (263 K–303 K).

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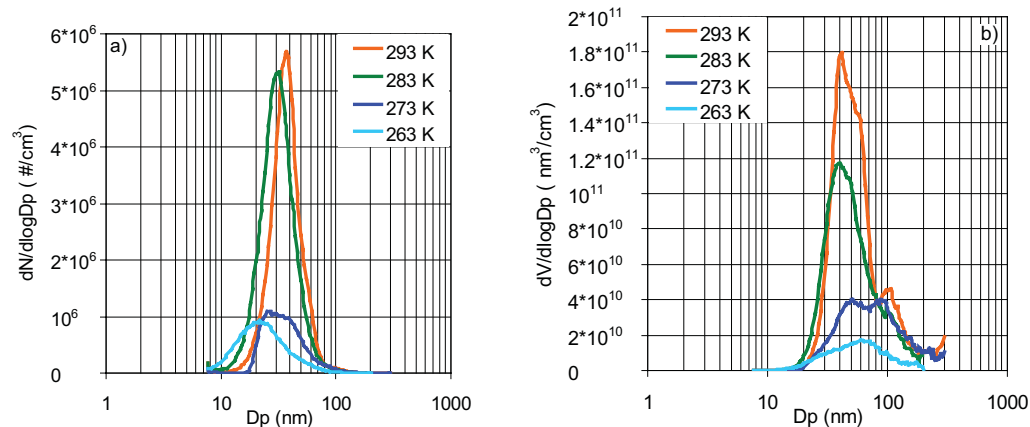
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**Fig. 3.** Particle number **(a)** and volume **(b)** size distributions from humid experiments with  $[\beta\text{-pinene}]_0 = 0.97\text{ ppmv}–1.76\text{ ppmv}$  and  $[\text{O}_3]_0 \approx 1.25\text{ ppmv}$  (except for 263 K:  $[\text{O}_3]_0 = 0.9\text{ ppmv}$ ) at different temperatures (263 K–293 K).

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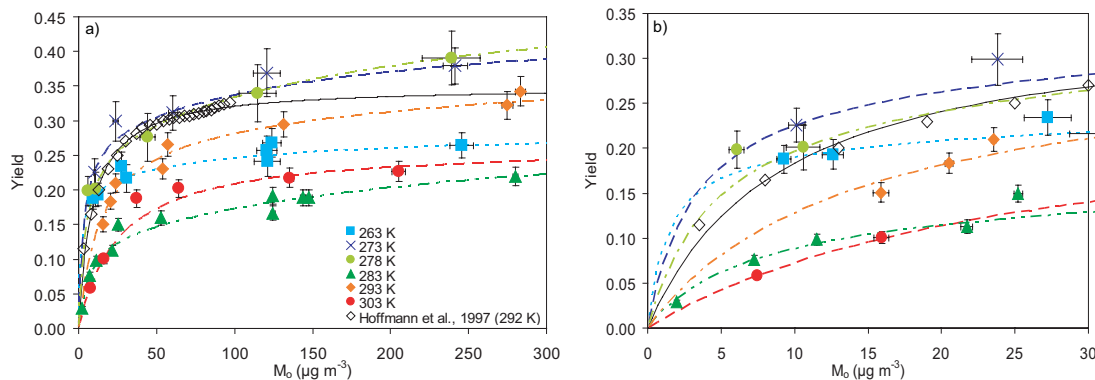
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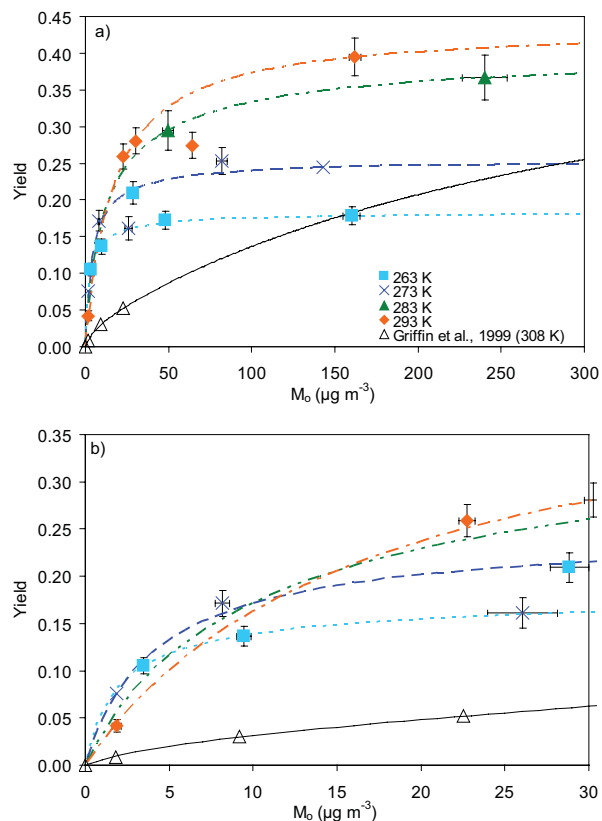


**Fig. 4.** Secondary organic aerosol yield ( $Y$ ) plotted against mass concentration of organic particulate matter ( $M_o$ ) from dry experiments performed at different temperatures (263 K–303 K): **(a)** all data from this study (Table 1), and Hoffmann et al. (1997); **(b)** blow-up of low  $M_o$  range from Fig. 4a. Symbols and error bars represent the arithmetic mean and standard deviations of 4–24 replicate measurements performed in each experiment. Lines represent two-product model “B fits” (Table 5).

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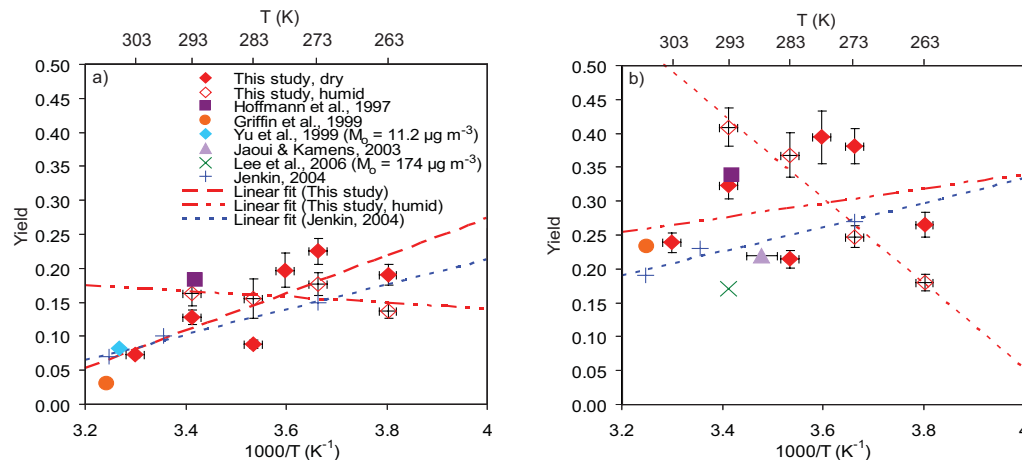
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**Fig. 5.** Secondary organic aerosol yield (Y) plotted against mass concentration of organic particulate matter ( $M_o$ ) from humid experiments performed at different temperatures (263 K–293 K): **(a)** all data from this study (Table 2), and Griffin et al. (1999); **(b)** blow-up of low  $M_o$  range from Fig. 5a. Symbols and error bars represent the arithmetic mean and standard deviations of 9–23 replicate measurements.

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**Fig. 6.** Secondary organic aerosol yield ( $Y$ ) plotted against inverse temperature ( $1000/T$ ): **(a)**  $M_o = 10 \mu\text{g m}^{-3}$ ; **(b)**:  $M_o = 250 \mu\text{g m}^{-3}$ . The symbols represent measurement or two-product model results of different studies. The error bars of the yield represent the standard deviations of 4–24 replicate measurements from our experiments with  $M_o$  close to  $10 \mu\text{g m}^{-3}$  or  $250 \mu\text{g m}^{-3}$  respectively. The error bars of the temperature represent the confidence interval of the thermo sensors applied in our study and the range of temperatures reported in other studies. Lines are linear fits.

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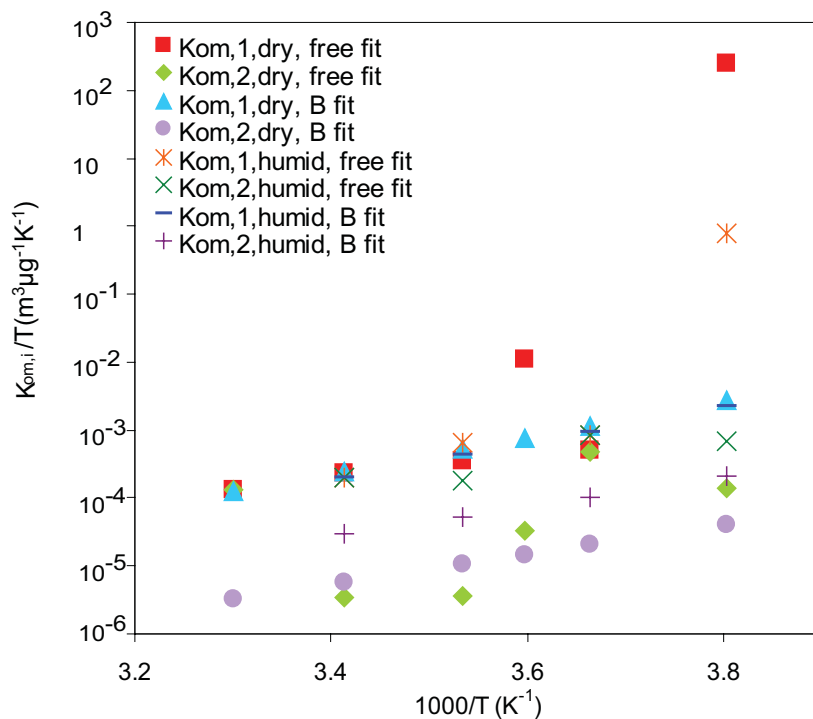
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**Fig. 7.** Temperature-normalized partitioning coefficients ( $K_{om,i}/T$ ) plotted against inverse temperature.

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